CLAIMS

Please amend the claims as follows:

- 1. (original) A melt phase process for making a polyester polymer melt phase product containing at least 100 ppm antimony based on the weight of the product comprising adding an antimony containing catalyst to the melt phase; polycondensing a melt containing said catalyst in a polycondensation zone; and before the lt.V. of the melt reaches 0.45 dL/g, continuously polycondensing the melt in the polycondensation zone at a temperature within a range of 265°C to 305°C or at sub-atmospheric pressure or a combination thereof, in each case until the lt.V. of the melt reaches at least 0.75 dL/g; wherein the polyester polymer melt phase product has a b* color of -5 to +5.
- 2. (original) The process of claim 1, wherein said polyester polymer melt phase product comprises :
 - (a) a carboxylic acid component comprising at least 60 mole% of the residues of terephthalic acid, derivates of terephthalic acid, naphthalene-2,6-dicarboxylic acid, derivatives of naphthalene-2,6-dicarboxylic acid, or mixtures thereof, and (b) a hydroxyl component comprising at least 60 mole% of the residues of ethylene glycol,

based on 100 mole percent of carboxylic acid component residues and 100 mole percent of hydroxyl component residues in the polyester polymer melt phase product.

- 3. (original) The process of claim 2, wherein the polyester polymer melt phase product comprises:
 - (a) a carboxylic acid component comprising at least 60 mole% of the residues of terephthalic acid or derivates of terephthalic acid, based on 100 mole percent of carboxylic acid component residues in the product.
- 4. (original) The process of claim 3, wherein the polyester polymer melt phase product comprises:
 - (a) a carboxylic acid component comprising at least 92 mole% of the residues of terephthalic acid or derivates of terephthalic acid, and

(b) a hydroxyl component comprising at least 92 mole% of the residues of ethylene glycol,

based on 100 mole percent of carboxylic acid component residues and 100 mole percent of hydroxyl component residues in the polyester polymer melt phase product.

- 5. (original) The process of claim 1, wherein the polycondensation reaction in the polycondensation zone is conducted in the absence of active catalysts containing titanium.
- 6. (original) The process of claim 5, wherein the melt phase process is conducted in the absence of added catalyst compounds containing titanium.
- 7. (original) The process of claim 6, wherein the melt phase product contains 180 ppm to 500 ppm antimony.
- 8. (original) The process of claim 1, wherein said polycondensation reaction is conducted for less than 100 minutes in a finishing zone.
- 9. (original) The process of claim 8, wherein said polycondensation reaction is conducted for 80 minutes or less in a finishing zone.
- 10. (original) The process of claim 1, comprising adding a phosphorus containing compound.
- 11. (original) The process of claim 10, wherein the phosphorous containing compound is added at a molar ratio of P:Sb of at least 0.025:1.
- 12. (original) The process of claim 1, comprising adding bluing toners to the melt phase.
- 13. (original) The process of claim 1, wherein said product has an L* of at least 70.
- 14. (original) The process of claim 13, wherein the L* color of the melt phase product is at least 74, and the b* color is between -5 and +4.
- 15. (original) The process of claim 1, wherein said polycondensation reaction in the polycondensation zone is conducted at a temperature of 280°C or more.
- 16. (original) The process of claim 15, wherein the product has an L* of at least 76 and the b* color is between -5 and +4.
 - 17. (Canceled)

- 18. (Canceled)
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- 39. (Canceled)
- 40. (original) A process for making a polyester polymer comprising polycondensing a melt in the presence of an antimony-containing catalyst to produce a melt phase product, wherein the reaction time of the melt between an It.V. of 0.45 dL/g to and It.V. ranging from 0.70 dL/g to 0.90 dL/g is 100 minutes or less.
- 41. (original) The process of claim 40, wherein a pressure applied between said range is about 2 mm Hg or less.
- 42. (original) The process of claim 40, wherein the melt phase product produced by said process has a b* within a range of -5 to +5.

- 43. (original) The process of claim 40, wherein the polyester polymer has an It.V. of at least 0.75 dL/g.
- 44. (original) The process of claim 40, wherein the reaction time of the melt between an It.V. of about 0.3 dL/g and an It.V. in the range of 0.70 dL/g to 0.90 dL/g is 100 minutes or less.
 - 45. (original) The process of claim 40, wherein the time is 80 minutes or less.
- 46. (original) A polyester polymer melt phase product having a degree of crystallinity of at least 25% and an It.V. of at least 0.70 dL/g without solid state polymerizing the polymer, said product comprising antimony residues and having a b* color of -5 to +5 and an L* of at least 70.
- 47. (original) The product of claim 46, wherein the polymer is substantially free of titanium residues.
 - 48. (original) The product of claim 46, wherein the L* is at least 74.
- 49. (original) The product of claim 46, wherein the degree of crystallinity is at least 30%.
- 50. (original) The product of claim 46, wherein the It.V. of the melt phase product is at least 0.75 dL/g.
- 51. (original) A melt phase process for making a polyester polymer melt phase product comprising adding an antimony containing catalyst to the melt phase, polycondensing a melt containing said catalyst in the melt phase until the lt.V. of the melt reaches at least 0.75 dL/g.
- 52. (original) The process of claim 51, wherein the polyester polymer melt phase product comprises:
 - (a) a carboxylic acid component comprising at least 60 mole% of the residues of terephthalic acid or derivates of terephthalic acid, based on 100 mole percent of carboxylic acid component residues in the product.
- 53. (original) The process of claim 51, wherein the polyester polymer melt phase product comprises:
 - (a) a carboxylic acid component comprising at least 92 mole% of the residues of terephthalic acid or derivates of terephthalic acid, and

(b) a hydroxyl component comprising at least 92 mole% of the residues of ethylene glycol,

based on 100 mole percent of carboxylic acid component residues and 100 mole percent of hydroxyl component residues in the polyester polymer melt phase product.

- 54. (original) The process of claim 51, wherein the polycondensation reaction in the polycondensation zone is conducted in the absence of active catalysts containing titanium.
- 55. (original) The process of claim 51, wherein the melt phase process is conducted in the absence of added catalyst compounds containing titanium.
- 56. (original) The process of claim 55, wherein the melt phase product contains 180 ppm to 500 ppm antimony.
- 57. (original) The process of claim 51, wherein said polycondensation reaction is conducted for less than 100 minutes in a finishing zone.
- 58. (original) The process of claim 57, wherein said polycondensation reaction is conducted for 80 minutes or less in a finishing zone.
- 59. (original) The process of claim 51, comprising adding a phosphorus containing compound.
- 60. (original) The process of claim 59, wherein the phosphorous containing compound is added at a molar ratio of P:Sb of at least 0.025:1.
- 61. (original) The process of claim 51, comprising adding bluing toners to the melt phase.
- 62. (original) The process of claim 51, wherein said product has an L* of at least 70.
- 63. (original) The process of claim 62, wherein the L* color of the melt phase product is at least 74, and the b* color is between -5 and +4.
- 64. (original) The process of claim 51, wherein said polycondensation reaction in the polycondensation zone is conducted at a temperature of 280°C or more.
- 65. (original) The process of claim 64, wherein the product has an L* of at least 76 and the b* color is between -5 and +4.
 - 66. (Canceled)

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